IN THE CLAIMS

Please amend the claims as follows:

1. (Currently Amended) A water treatment apparatus comprising

a plurality of composite reverse osmosis membrane modules arranged in multi-stages,

each of the plurality of modules including a porous support and a polyamide skin layer formed on the porous support,

the plurality of modules including a final-stage module and at least one pre-final module, wherein the polyamide skin layer in the at least one pre-final module comprises bromine atoms,

wherein a selected portion of permeated water obtained from the at least one pre-final module is supplied to the final-stage module, and

a rest of the permeated water is discharged from or recovered in the apparatus along with permeated water obtained from the final-stage module.

2. (Original) Thewater treatment apparatus according to claim 1,

wherein the permeated water from the final-stage module and the permeated water that is not supplied from the at least one pre-final module to the final-stage module are mixed with each other to be discharged or recovered.

3. (Previously Amended) The water treatment apparatus according to claim 1,

wherein a ratio (A : B) of an ion concentration (A) of the permeated water supplied to the final-stage module and an ion concentration (B) of the permeated water

that is not supplied to the final-stage module is in a range of 2 : 1 to 10 : 1.

4. (Original) The water treatment apparatus according to claim 1,

wherein the permeated water supplied to the final-stage module is adjusted to be alkaline.

5. (Original) The water treatment apparatus according to claim 4,

wherein a pH of the permeated water supplied to the final-stage module is in a range of 8 to 12.

6. (Original) The water treatment apparatus according to claim 1,

wherein the permeated water supplied to the final-stage module is discharged from a concentrate side of at least one pre-final module supplying the permeated water to the final-stage module.

7. (Original) The water treatment apparatus according to claim 1 further comprising

a pressure vessel

wherein a plurality of pre-final modules are provided as the at least one pre-final module,

each of the plurality of pre-final modules is a spiral module formed by winding a composite reverse osmosis membrane around a water-collecting pipe,

the plurality of pre-final modules are connected with each other by connecting their water-collecting pipes,

the plurality of pre-final modules thus connected are contained in the pressure vessel,

raw water to be treated is supplied to and permeated water is discharged from one end of the pressure vessel,

concentrated water and permeated water are discharged from the other end of the pressure vessel, and

the permeated water discharged from the other end is supplied to the final-stage module.

8. (Original) The water treatment apparatus according to claim 7,

wherein an interior space of the connected water-collecting pipes is divided into two separate spaces by a partition to separate permeated water on a raw water side and permeated water on a concentrated side.

9. (Original) The water treatment apparatus according to claim 1 further comprising

a plurality of pressure vessels arranged in multi-stages,

the plurality of pressure vessels including a first-stage pressure vessel and at least one pressure vessel subsequent to the first-stage pressure vessel,

wherein a plurality of pre-final modules are provided as the at least one pre-final module,

each of the plurality of pre-final modules is a spiral module formed by winding a composite reverse osmosis membrane around a water-collecting pipe,

the plurality of pre-final modules are connected with each other by connecting

their water-collecting pipes,

the plurality of pre-final modules thus connected are contained in the plurality of pressure vessels,

the first-stage pressure vessel is supplied with raw water to be treated,

the at least one pressure vessel subsequent to the first-stage pressure vessel is supplied with concentrated water discharged from at least one preceding pressure vessel, and

the final-stage module is supplied with permeated water discharged from the at least one pressure vessel subsequent to the first-stage pressure vessel.

10. (Original) The water treatment apparatus according to claim 9,

wherein three pressure vessels are arranged in three stages, and

permeated water from a second-stage pressure vessel and/or a third-stage pressure vessel is supplied to a final-stage composite reverse osmosis membrane.

11. (Original) The water treatment apparatus according to claim 1,

wherein the at least one pre-final module has a salt rejection of at least 99% and a permeate flux of at least $0.2m^3/m^2 \cdot day$ when the apparatus is operated using as a feed solution a 3.5wt% salt water at a pH of 6.5, a water temperature of 25°C, and an operational pressure of 5.5Mpa.

12. (Original) The water treatment apparatus according to claim 1,

wherein the at least one pre-final module has a salt rejection of at least 99.5% and

a permeate flux of at least $0.3m^3/m^2 \cdot day$ when the apparatus is operated using as a feed solution a 3.5wt% salt water at a pH of 6.5, a water temperature of 25°C, and an operational pressure of 5.5Mpa.

13. (Original) The water treatment apparatus according to claim 1,

wherein the at least one pre-final module has a boron rejection of at least 80% when the apparatus is operated using as a feed solution a 3.5wt% salt water containing 5ppm of boron at a pH of 6.5, a water temperature of 25°C, and an operational pressure of 5.5Mpa.

14. (Original) The water treatment apparatus according to claim 1,

wherein the at least one pre-final module has a boron rejection of at least 90% when the apparatus is operated using as a feed solution a 3.5wt% salt water containing 5ppm of boron at a pH of 6.5, a water temperature of 25°C, and an operational pressure of 5.5Mpa.

15. (Original) The water treatment apparatus according to claim 1,

wherein the final-stage module has a salt rejection of at least 98% and a permeate flux of at least $0.5m^3/m^2 \cdot day$ when the apparatus is operated using as a feed solution a 0.05wt% salt water at a pH of 6.5, a water temperature of 25°C, and an operational pressure of 0.75Mpa.

16. (Original) The water treatment apparatus according to claim 1,

wherein the final-stage module has a salt rejection of at least 99.0% and a permeate flux of at least $0.7m^3/m^2 \cdot day$ when the apparatus is operated using as a feed solution a 0.05wt% salt water at a pH of 6.5, a water temperature of 25°C, and an operational pressure of 0.75Mpa.

17. (Original) The water treatment apparatus according to claim 3,

wherein a concentration of total dissolved solids (TDS) in the raw water supplied to the apparatus is at least 1wt%.

18. (Original) The water treatment apparatus according to claim 17,

wherein the raw water supplied to the apparatus is seawater.

19. (Original) The water treatment apparatus according to claim 3,

wherein the raw material supplied to the apparatus is seawater, and a concentration of boron in permeated water discharged from or recovered in the apparatus is 1mg/l or less.

20. (Cancelled)